

**PRELIMINARY RESULTS OF
LES SIMULATIONS OF
SELF-SIMILAR VARIABLE
ACCELERATION RT MIXING FLOWS**

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The importance of self-similar variable acceleration RT flows (SSVARTs) for the design and calibration of turbulent mixing models is shown in the presentation by Antoine Llor at this workshop.

Because experimental results on SSVARTs are not, and will probably not be available in the near future, we are currently investigating such flows by means of LES.

In these incompressible flows the acceleration has the form

$$g = kt^n$$

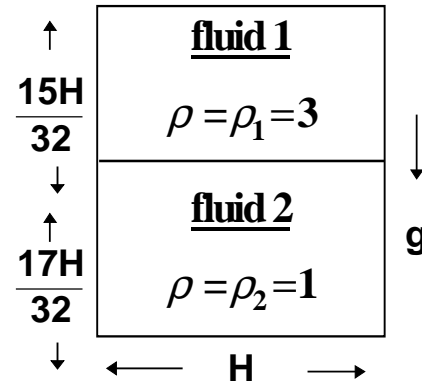
and for self-similar mixing the mixing zone width grows in proportion to t^{n+2} .

Preliminary results, using low-resolution LES are given for $n = 0, 1$ and -1 , using the TURMOIL3D code.

Results are compared with simple theoretical models.

THE TEST PROBLEM

This is based on the test problem proposed by Guy Dimonte (see presentation at this workshop).



Computational domain	:	H x H x 2H
Zoning	:	128 x 128 x 256
Dimension	:	H = 1
Acceleration	:	(a) g = 2 (b) g = t (c) g = 9/(4t)

Run to $t = 4.5$, when for each case

$$\left(\int \sqrt{g} dt\right)^2 = 40.5$$

Compressible calculation with Mach number < 0.2

The major calculational problem is the treatment of variable g within a compressible calculation.

For incompressible flow, the pressure distribution adjusts at each instant of time to maintain $\text{div } \underline{u} = 0$. If no mixing occurs this implies hydrostatic equilibrium.

$$\frac{\partial p}{\partial z} = \rho g$$

In the compressible simulations an appropriate pressure gradient is maintained by adding an internal energy source.

Initially adiabatic hydrostatic equilibrium (uniform entropy/neutral stability within each fluid) is assumed:-

$$\frac{\partial p_0}{\partial z} = \rho_0 g_0$$

$$p_0 = k \rho_0^\gamma \quad , \quad \text{in each region}$$

$$\rho_0 = \begin{cases} 3 & \text{just above the interface} \\ 1 & \text{just below the interface} \end{cases}$$

$$\gamma = \frac{5}{3} \quad \text{for both fluids}$$

If $g_{n+\frac{1}{2}}$ is the value of g for the n -th time step, at the start of the time step

the internal energy is scaled:-

$$\varepsilon' = \varepsilon \cdot \frac{g_{n+\frac{1}{2}}}{g_{n-\frac{1}{2}}}$$

This maintains hydrostatic equilibrium outside the mixing zone and uniform entropy within each fluid.

The acceleration history needs to be modified slightly to give finite non-zero g at $t = 0$:-

case (b) $g = \max \{0.01, t\}$

case (c) $g = \min \{50, 9/(4t)\}$

The initial interface pressure is chosen high enough to ensure that the Mach no. of the flow remains small ($M < 0.2$) at all times and also high enough to give small (<4%) variation in the initial density of each region.

THE INITIAL PERTURBATION

RT experiments with constant g give bubble penetration

$$h_1 = \alpha \frac{\rho_1 - \rho_2}{\rho_1 + \rho_2} g t^2 \quad , \text{ with } \alpha \sim 0.05 \text{ to } 0.06$$

TURMOIL3D calculations with short wavelength initial perturbations (growth purely by mode coupling) give $\alpha \sim 0.03$.

Need to assume long wavelength initial perturbations with amplitude \propto wavelength (as proposed by Inogamov [1]) to give self-similar growth with $\alpha \sim 0.05$.

Perturbation used $\xi(x,y) = \xi_S + \xi_L$

ξ_S : wavelenghts $4\Delta x$ to $8\Delta x$
s.d = $0.02 \Delta x$

ξ_L : power spectrum $P(k)$

$$\sigma_\lambda = \left\{ \int_{2\pi/\lambda}^{\infty} P(k) dk \right\}^{\frac{1}{2}} = \varepsilon \lambda$$

$$\Rightarrow P(k) \propto 1/k^3$$

$$\varepsilon = 0.0005$$

wavelenghts in the range $4\Delta x$ to $\frac{H}{2}$

RESULTS SHOWN

f_1 , f_2 : volume fractions of fluids 1 and 2

\bar{f}_1 , \bar{f}_2 : plane averaged values

$W = \int \bar{f}_1 \bar{f}_2 dz$ integral mix width

h_1 : bubble penetration - measured to point where $\bar{f}_1 = 0.99$.
Approximation used here : $h_1 = 3.3W$

$\theta = \frac{\int \bar{f}_1 \bar{f}_2 dz}{\int \bar{f}_1 \cdot \bar{f}_2 dz}$, molecular mixing fraction

$\frac{D}{P} = \frac{\text{KE dissipated}}{\text{KE production}}$

$S = \frac{\rho_1 - \rho_2}{\rho_1 + \rho_2} \left(\int \sqrt{g} dt \right)^2$

Fig 1 : initial long wavelength perturbation

Fig 2 : isosurfaces for the case $g = k$

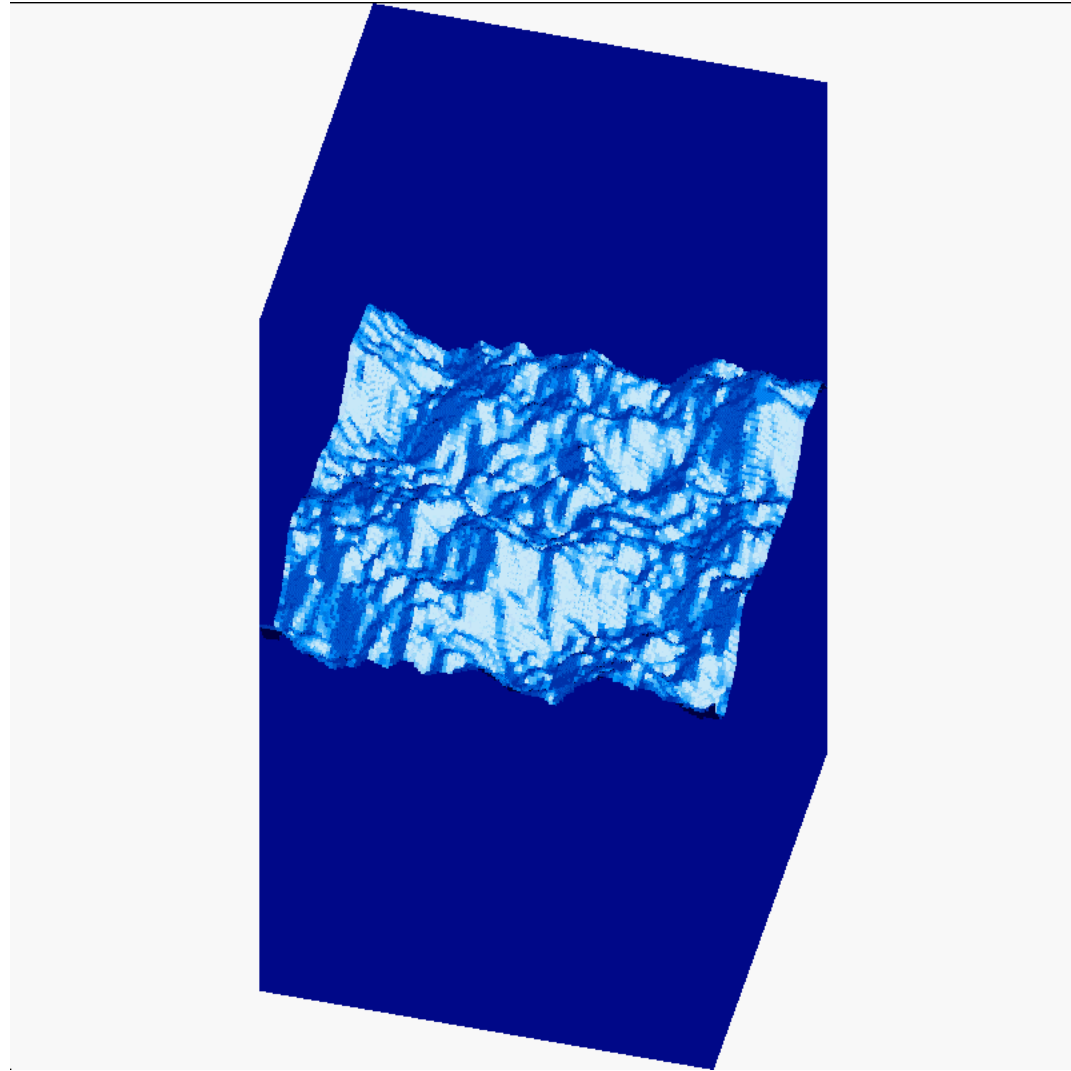
Fig 3 : profiles of \bar{f}_1

Fig 4 : plots of h_1

Fig 5 : plots of θ

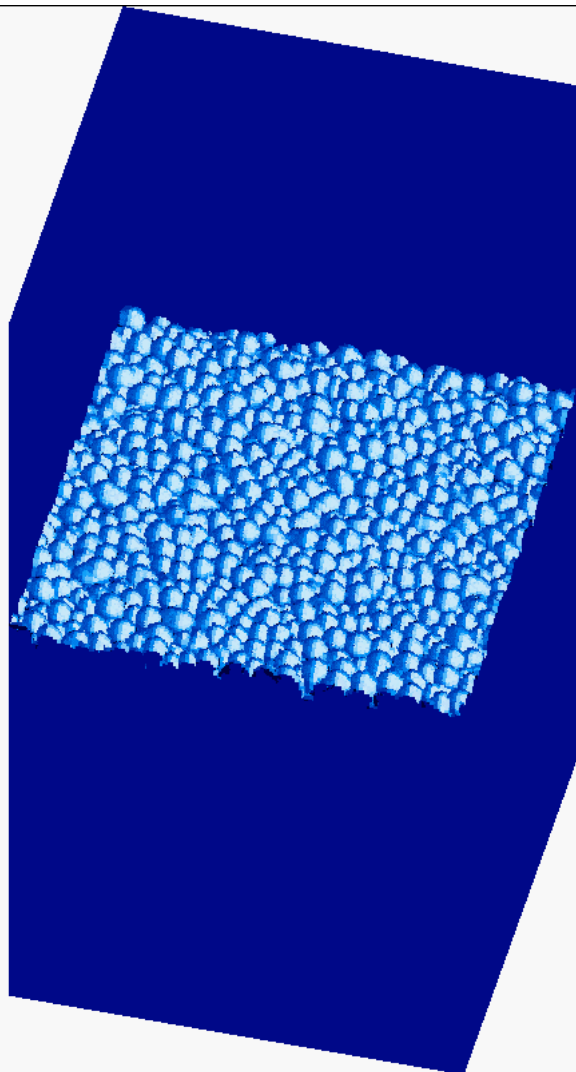
Fig 6 : plots of D/P

Figure 1

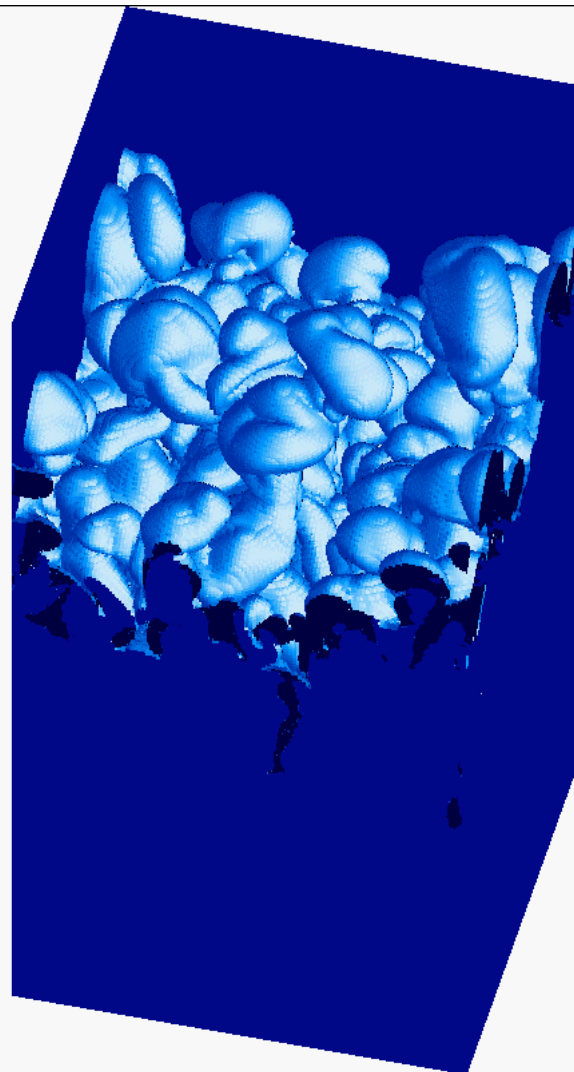


$\epsilon = 0.005$, initial perturbation x 200

Figure2: Isosurfaces ($f_1 = 0.99$) for $g = k$



$t = 0.9$



$t = 3.5$

Figures3

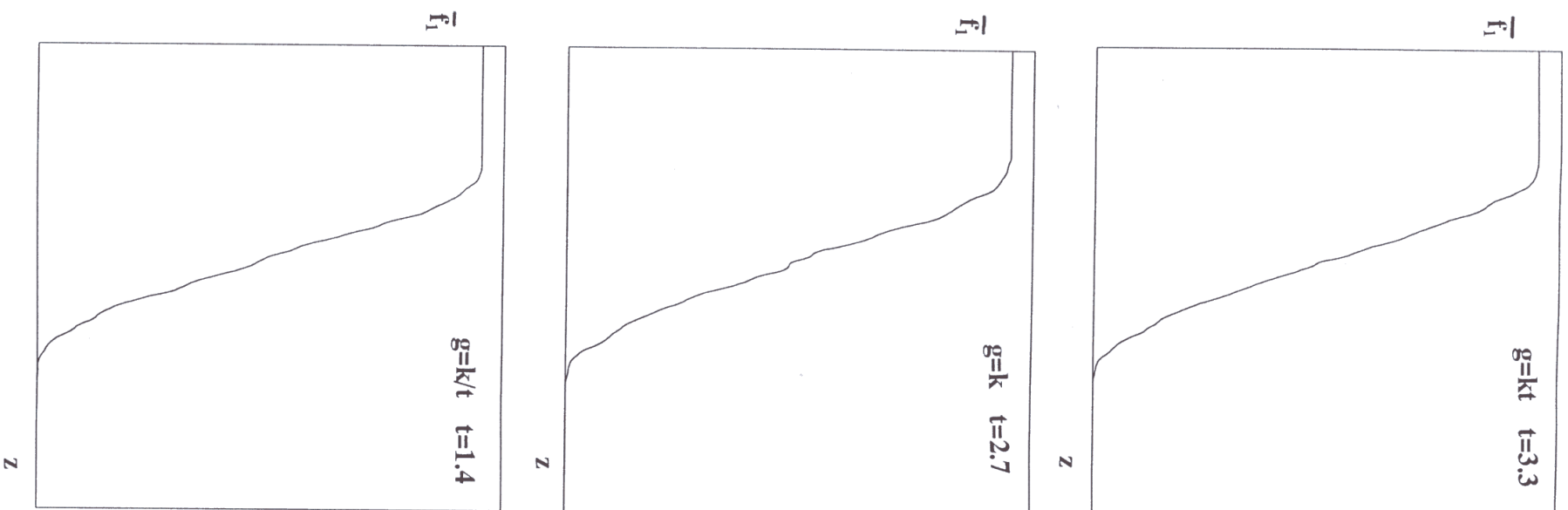


Figure4

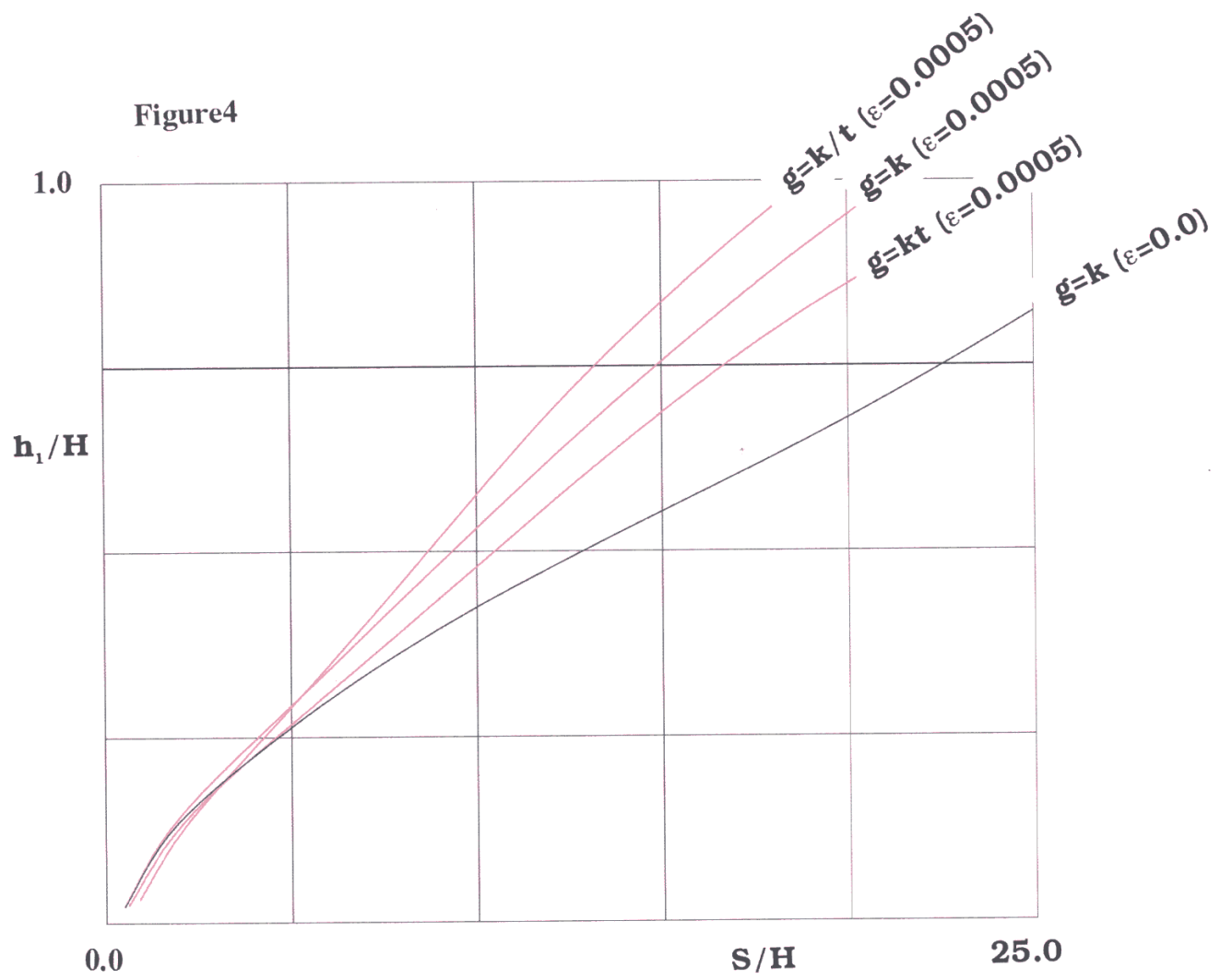


Figure5

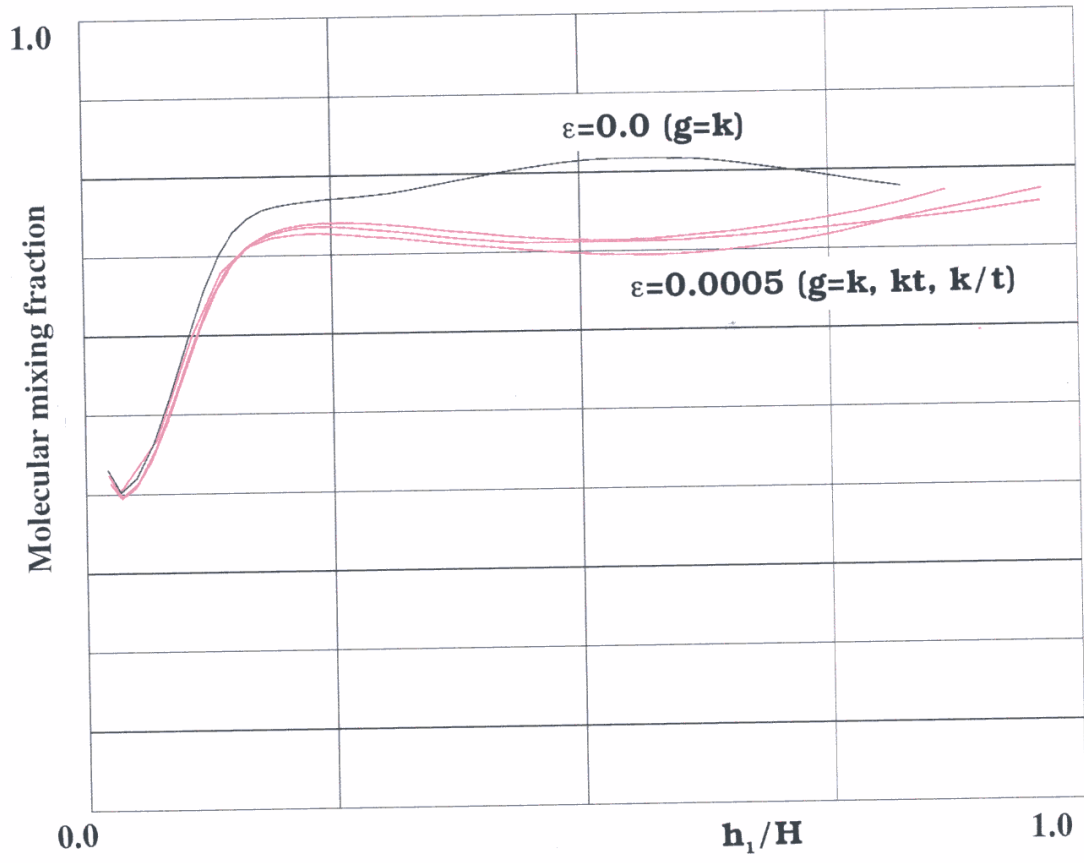
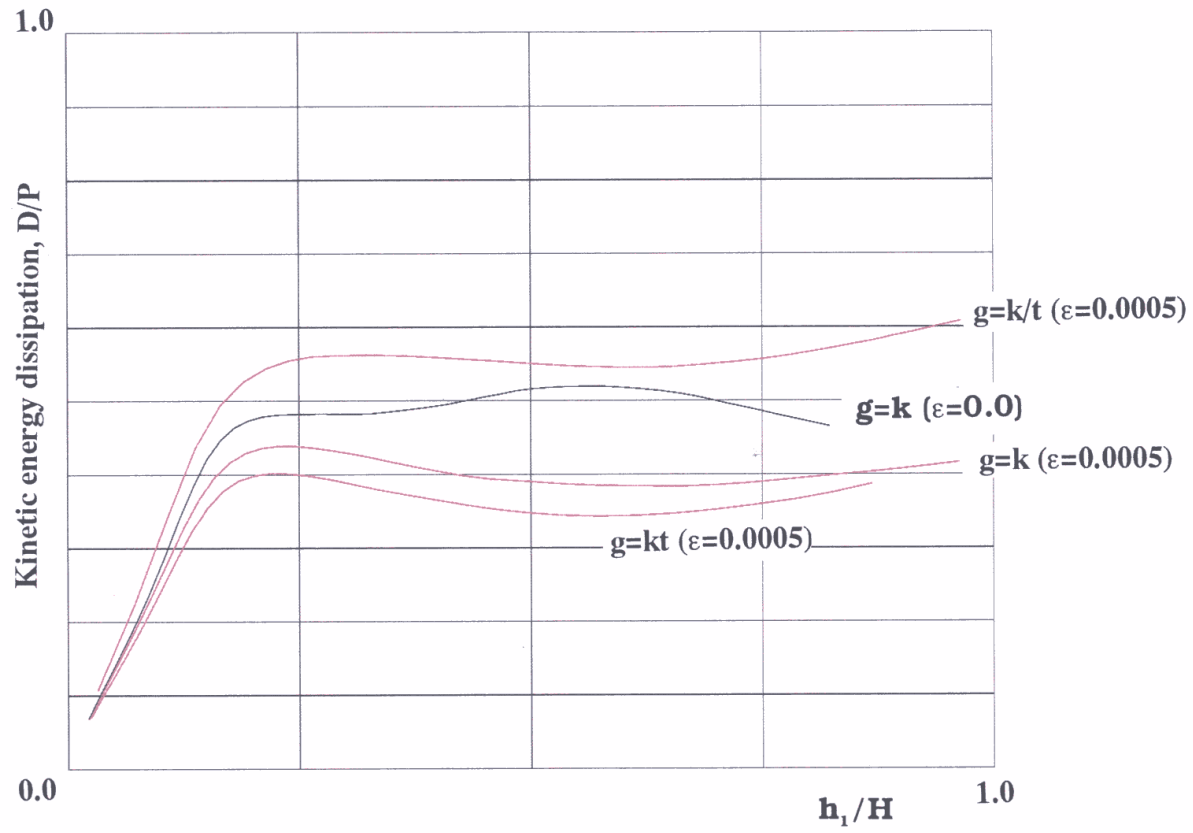
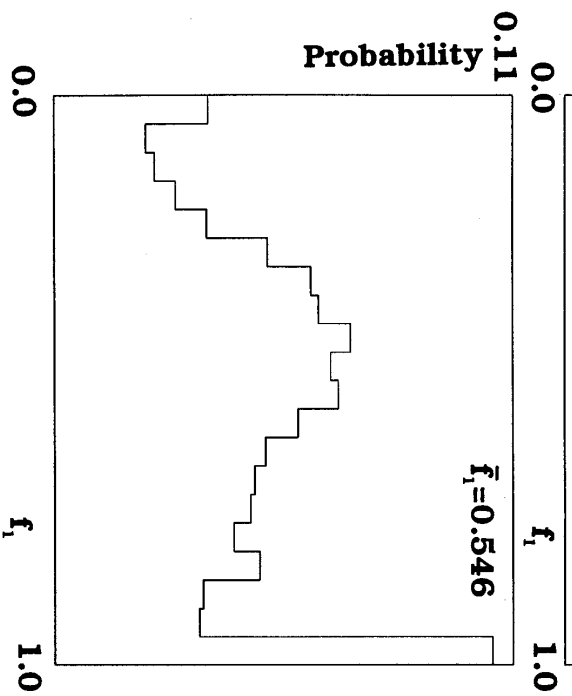
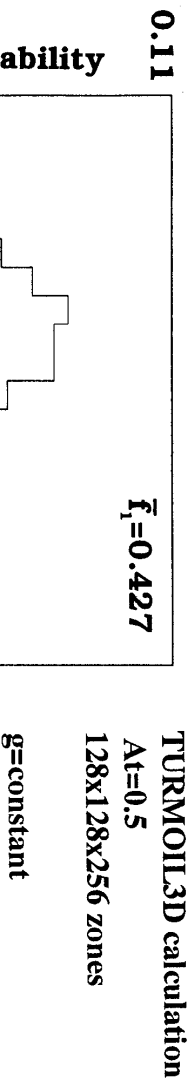
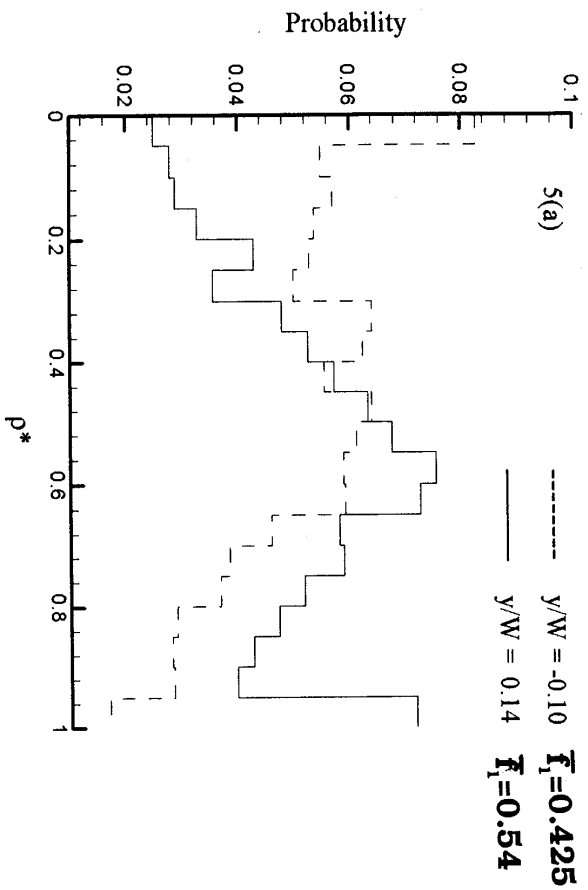


Figure6



**Figure7 : Probability distributions for f_1 within a plane
z=constant**

Wilson and Andrews At =0.001



COMPARISON OF RESULTS WITH SIMPLE MODELS

(A) The Simplest Model

Bubbles of radius R have a limiting velocity $\sim \sqrt{AgR}$. If it is assumed that $R \sim h_1$, then

$$\dot{h}_1 = c\sqrt{Agh_1}$$

$$\text{ie } h_1 = \alpha A \left\{ \int_0^t \sqrt{g(t')} dt' \right\}^2 = \alpha S \quad \dots(1)$$

Figure 5 shows plots of h_1 vs S . The slopes of the curves (for the range $h_1/H = 0.25$ to 0.75) give; for $\varepsilon = 0.0005$

$n = 0$,	α	=	0.0464
$n = 1$,	α	=	0.0415
$n = -1$,	α	=	0.0559

The model works surprisingly well, but there is some variation of α with n :-

$$\frac{\alpha_1}{\alpha_0} = 0.89$$

$$\alpha_0$$

$$\frac{\alpha_{-1}}{\alpha_0} = 1.20$$

$$\alpha_0$$

(B) A Buoyancy - Drag Model

A model of this type, based on a modified form of Layzer's equation for a bubble rising in a cylindrical tube, was used by Hansom et al [2].

$$\ddot{h}_1 = Ag - \frac{C_D (\dot{h}_1)^2}{h_1} \quad \dots (2)$$

acceleration = buoyancy - drag

For constant g , $C_D = 4.5$ gives $\alpha = 0.05$. Then if α is defined as in equation (1):-

$$\frac{\alpha_1}{\alpha_0} = 0.97$$

$$\frac{\alpha^{-1}}{\alpha_0} = 1.11$$

This is closer to the TURMOIL3D results than taking α independent of n but the change is not large enough.

Dimonte and Schneider [3] include a factor $\beta < 1$ in front of the Ag term in equation (2). This improves agreement with the 3D simulations.

(C) An Energy Balance Model

This is version of the model proposed by Ramshaw [4], but with different settings for the model coefficients.

Let $K = \frac{1}{2}(\rho_1 + \rho_2) h_1 V^2$ = kinetic energy within the mixing layer.

\dot{P} = KE production rate (loss of potential energy)

\dot{D} = dissipation rate

Then the model equations used are

$$\dot{K} = \dot{P} - \dot{D}$$

$$\dot{P} = c_1(\rho_1 - \rho_2) g h_1 \dot{h}_1$$

$$\dot{D} = c_2 \frac{1}{2}(\rho_1 + \rho_2) V^3$$

$$\dot{h}_1 = c_3 V$$

The coefficient c_1 depends on the shape of the volume fraction profile. For a linear distribution $c_1 = 1/3$. For the TURMOIL3D profiles (figure 4) $c_1 = 0.30$, and this is the value used here.

If for constant g we assume, $\alpha = 0.05$ and $D/P = 0.4$ (figure 7) then

$$c_2 = 1.4055$$

$$c_3 = 1.0541$$

The equation $\dot{K} = \dot{P} - \dot{D}$ gives

$$\begin{aligned}\ddot{h}_1 &= c_1 c_3^2 Ag - \frac{c_2 + c_3}{2c_3} \frac{(\dot{h}_1)^2}{h_1} \\ &= \frac{1}{3} Ag - \frac{7}{6} \frac{(\dot{h}_1)^2}{h_1} \quad \dots (3)\end{aligned}$$

This has the same form as the buoyancy - drag model (2). The coefficient in front of the Ag term is less than unity as in Dimonte and Schneider [3].

This choice of the coefficients gives

$$\frac{\alpha_1}{\alpha_0} = 0.91$$

$$\frac{\alpha_{-1}}{\alpha_0} = 1.43$$

also	D/P	=	0.40 assumed for n = 0
	D/P	=	0.36 for n = 1
	D/P	=	0.57 for n = -1

α_1/α_0 agrees with the 3D simulations

α_{-1}/α_0 appears to be somewhat too high. However, the variation of D/P with n (see fig. 6) is represented very well.

FUTURE PLANS

- Values of n outside the range $[-1, 1]$**
- Higher resolution TURMOIL3D calculations**
- Use of the SSVARTs results to differentiate between various types of RANS models.**

REFERENCES

- 1. N A Inogamov et al, Proceedings of the 3rd IWPC TM, Royaumont (1991)**
- 2. J C V Hansom et al, Laser and Particle Beams, Vol 8, p 51 (1990)**
- 3. G Dimonte and M Schneider, Phys Rev E54, p 3740 (1996)**
- 4. J D Ramshaw, Phys Rev E58, p 5834 (1998)**