DEVELOPMENT AND VALIDATION OF A 2D TURBULENT MIX MODEL

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Problems of interest

- Compressible flow with interfaces between fluids of widely differing densities.
- High Reynolds No.
- Turbulent mixing at interfaces. Due to RT instability, RM instability. KH instability also important.

Need to model turbulent mixing in flows which are on average 1D or 2D.

Strategy for Numerical Simulation

- 3D Large Eddy Simulation (LES) impractical for real complex applications but can be successfully applied to simplified problems.
- High-resolution 3D LES is applied to simplified problems for which experimental results are available.
- A combination of 3D simulation results and experimental data is then used to set model coefficients used in a turbulence model (RANS model).
- The turbulence model is used to calculate the average mixing behaviour in 1D and 2D numercial simulations of complex real applications.

TURMOIL 3D

- Simple 3D compressible Eulerian hydrocode used for turbulent mixing studies (LES).
- Same numerical method as the AWE 2D and 3D Eulerian production codes, but without interface tracking.
- Moving mesh option:-



Used for shock tube applications

• Explicit numerical method ideally suited to parallelisation. Low Mach no. calculations used to approximate incompressible flow.

- Lagrangian phase non-dissipative except in the presence of shocks. Quadratic artifical viscous pressure used.
- Rezone or Advection phase.
 Monotonic advection method of Van Leer used for all fluid variables.
- Monotonic advection considered essential for problems considered here with shocks and initial density continuities.
 ⇒ non-linear dissipation at high wave numbers.
- Example of MILES (Monotone Integrated Large Eddy Simulation).
- No need for an additional sub-grid dissipation model.

THE 2D TURBULENCE MODEL (RANS MODEL)

Implemented in a 2D Eulerian hydrocode (which also has the moving mesh option)

Novel form of turbulence model - based on modelling the dynamics of the large scale structures (bubbles of light-fluid, drops of heavy fluid) rather than 1st or 2nd order closure assumptions for the fluctuating quantities)

Combines three basic ideas

- 1. Mixing induced by a pressure gradient or shock on fluids of different density.
- 2. Turbulent diffusion in the presence of concentration gradients.
- 3 Exchange of mass between the initial fluids is used to model the decay of concentration fluctuations [2].

Uses multiphase flow equations with turbulent diffusion terms added [1].

Bouyancy - drag model used to calculate initial behaviour - approximate representation of the initial conditions[3].

References: 1. D.L.Youngs, Laser and Particle Beams, vol 12, p725 (1994) 2. D.L. Youngs, Proceedings of 5th IWPCTM, Stony Brook(1995) 3. J.C.V. Hansom et al., Laser and Particle Beams, vol 8, p51(1990) The simple incompressible RT problem $(\rho_1, \rho_2, \text{g constant})$ is the key problem for fixing the turbulence model coefficients.

Loss of memory of initial conditions tends to occur \rightarrow self-similar mixing with length scale gt²:

Bubble penetration
$$h_1 = \alpha \frac{\rho_1 - \rho_2}{\rho_1 + \rho_2} gt^2$$

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 α ~ 0.05 to 0.06
 (AWRE Foulness, LLNL (LEM), Chelyabinsk 70)
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TURMOIL3D calculations with short-wavelength initial perturbations (growth purely by mode coupling) give $\alpha \sim 0.03$, less than observed.

Need to add long wavelength initial perturbations:-

$$\sigma^{2} = \int_{0}^{\infty} \mathbf{P}(\mathbf{k}) \, \mathbf{dk}$$

where $\left\{ \int_{2\pi/\lambda}^{\infty} \mathbf{P}(\mathbf{k}) \, \mathbf{dk} \right\}^{\frac{1}{2}} = \varepsilon \, \lambda$

 ϵ = 0.0005 gives self-similar growth with α ~ 0.05. It is assumed that this corresponds to a typical experimental situation.

Model coefficients are chosen to fit the key quantities for RT mixing

- α : growth rate coefficient
- D _ turbulence KE dissipated
- **P** : Loss of potential energy
- θ : molecular mixing fraction

$$\frac{\int \overline{f_1 f_2} dz}{\int \overline{f_1. \overline{f_2}} dz}$$

Values used are based on TURMOIL3D calculations (800 x 400 x 400 zones, $\epsilon = 0.0005$): -

α	=	0.05
D/P	=	0.4 (no experimental data)
θ	=	0.7 (some experimental confirmation)

Still leaves one key degree of freedom

$$\Delta = \frac{\Delta \mathbf{u}_{\mathsf{D}}}{\Delta \mathbf{u}_{\mathsf{D}} + \Delta \mathbf{u}_{\mathsf{P}}}$$

 $\Delta u_{p} =$ mixing velocity due to turbulent diffusion

 $\Delta u_{P} =$ mixing velocity induced by pressure gradient

Results shown here for $\Delta = 0.4$

TYPICAL 2D TURBULENCE MODEL APPLICATION



Points of concern

- (a) Likely to be some overlap between the mean flow scales and the turbulence scales is double counting an issue?
- (b) Some of the turbulence scales are resolved (but only in 2D). Does this matter?
- (c) Does the turbulence model give the correct spatial distribution in a complex 2D situation.

RAYLEIGH-TAYLOR EXPERIMENT (CAMBRIDGE UNIVERSITY) Dalziel, Linden, Youngs, JFM 1999



- 3D calculation : 400 x 320 x 160 zones Random perturbation ($\varepsilon = 0.0005$) removal \Rightarrow 2D on average 2D initial velocity field used to represent effect of barrier
- 2D turbulence model calculation 100 x 80 zones barrier perturbation included

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Initial velocity field (2D)

Model for barrier perturbation

2D turbulence model calculation – run to t=0.5 with interface tracking and initial conditions model.





Experiment (lower half of tank)

3D Numerical Simulation (200x160x80 zones)





T=3.0



3D simulation at t = 2.0 2D turbulence model at t = 2.0

Mean volume fraction contours: 0.05, 0.25, 0.75, 0.95



3D simulation at t = 3.0 2D simula

2D simulation at t = 3.0



Moving mesh option used (semi-Lagrangian calculations)

3D LES:400 x 320 x 160 zones
random interface perturbations (models effect of membrane
rupture)
wavelengths0.5 to 5 cm
s.d0.01 cm

2D turbulence model calculation

200 x 160 zones initial conditions model $a_o = 0.02 \text{ cm}, \quad \lambda_o = 0.5 \text{ cm}$





Experiment

3D simulation

3D simulation (scattered image)



3D simulation

Experiment

3D simulation(scattered image)



3D simulation at t = 2.0ms

2D turbulence model at t = 2.0ms

Double bump experiment

mean volume fraction contours: 0.05, 0.3, 0.7, 0.95



3D simulation at t = 3.0ms

2D turbulence model at t = 3.0ms



3D simulation at t = 4.0ms

2D turbulence model at t = 4.0ms



3D simulation at t = 2.0ms 2D turbulence model at t = 2.0ms

mean volume fraction contours: 0.05, 0.3, 0.7, 0.95

Chevron experiment



3D simulation at t = 3.0ms

2D turbulence model at t = 3.0ms



3D simulation at t=4.0ms

2D turbulence model at t=4.0ms

FINAL REMARKS

• The 2D turbulence model based on the equations of multiphase flow, using a single set of model coefficients has given satisfactory results for

RT self-similar mixing A 2D RT experiment The double-bump shock tube experiment The chevron shock tube experiment

- 3D LES for simplified problems, in conjunction with experimental data, is making a very valuable contribution to the validation of the turbulence model.
- In the near future (after AWE's next supercomputer procurement) a more detailed comparison, (including 2D distributions of k and θ) will be made between the 2D turbulence model results and higher resolution LES.